

## An Economic Analysis of Small-Scale Standalone Photovoltaic System with Hydrogen Storage System

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### Abstract

This paper proposes design steps in obtaining the optimal size of a standalone photovoltaic (PV) system, which is able to meet a predetermined power load requirement. The keys of the system sizing are primarily to satisfy a specific load demand that depends on the power generated from the installed PV system and also to maintain hydrogen storage state of charge. A case study was conducted using Kuala Lumpur's meteorological data and a typical rural area load profile of 2.215 kWh. An economic analysis on the system was performed in order to determine system feasibility. The levelized cost of energy for the proposed system was RM1.98/kWh. However, the results showed that if the same configuration used absorbent glass mat (AGM) battery as the backup power supply, the system cost and levelized cost of energy is lower. Therefore, a sensitivity analysis of the electrolyzer and fuel cell efficiencies towards levelized cost of energy for the proposed system was executed. The result indicates that unless the efficiency of hydrogen storage technologies significantly increases in the future, the system will not be feasible to be implemented in Malaysia.

Keywords: Standalone power system, photovoltaic generation, hydrogen storage, battery, economic analysis.

### 1.0 INTRODUCTION

World's electricity production depends mostly on coal, oil, and natural gas as power supply. Due to limited reserves of fuels, unstable prices, and global warming risks, the interest in renewable energy (RE) sources is increasing significantly. Moreover, the use of RE proves that the dependency on fossil fuels is declining, since RE is environmental friendly, free, and abundantly available [1].

Among the alternative energy available in Malaysia, a photovoltaic (PV) system has a big potential for electricity generation. However, because of its variation in nature, a standalone photovoltaic (SAPV) system needs another power source to support the system to continuously supply the power. In most cases, an SAPV system uses a battery as a backup power supply at night or during low irradiation period. A properly designed SAPV with a battery system requires an adequate capacity of PV array and battery, suitable charge controller rating, and inverter rating. There are several technologies of battery suitable for SAPV system application, such as lead-acid battery, lithium-ion battery, flow battery, and nickel-cadmium battery. Lead-acid battery has been employed in RE applications for decades and successfully applied in an off-grid system. Among several types of lead-acid battery, absorbent glass mat, gel, and flooded batteries are the most commonly used [2]. Battery's cycle life depends on its depth of discharge, since the battery degrades as it is charged and discharged, and the discharge-recharge cycle is affected by the maximum depth of discharged. The higher the battery capacity is discharged each time it is used, the faster the battery degrades.

Other than battery, an SAPV system can also use a generator as a backup power supply. A generator is not only implemented as a backup power supply, but it can also be used as a supply for other loads that exceed inverter capacity [3]. However, similar to a battery, a generator is quite expensive, requires maintenance, and has low lifetime compared

to a PV system. Besides, it also creates noises when running and pollutes the environment.

Past literature also suggested a hybrid SAPV system coupled with other renewable energies, such as wind. A hybrid SAPV system with wind is highly recommended, since both sources are unlimited and can be installed anywhere (depending on site condition). A proper combination is able to overcome the shortcoming of their intermittency and unpredictable nature. However, an SAPV with wind system still needs to install an additional backup power, such as a battery and a generator, in order to provide more security and increase system reliability.

Recently, hydrogen storage system (HSS) has been receiving a lot of attention as an energy storage due to its regenerative hydrogen feature. Integrating PV with HSS leads to non-polluting and reliable energy sources, insightful environmental benefits, and reducing emissions. The introduction of HSS in the energy mix is one of the big steps to introduce hydrogen economy in a small-scale autonomous power application due to the high cost of energy produced by a conventional SAPV generation system.

In an SAPV system, hydrogen is produced from water by electrolysis process in an electrolyzer, powered by the excess electricity from PV generation. An electrolyzer decomposes water molecules into hydrogen and oxygen. The most common or preferable technologies used for water electrolysis are alkaline and proton exchange membrane electrolyzer (PEME). The advantage of PEME technology is that it has high energy efficiency for each stack (75–88%), whereas an alkaline electrolyzer has lower energy efficiency range (62–74%) [4]. The hydrogen produced is then stored in a hydrogen tank. When the load demand is higher than the generated PV energy, the stored hydrogen and air are fed into a fuel cell (FC) [5, 6]. Fuel cell is widely used to convert pure hydrogen into usable energy. It performs a reverse electrochemical reaction in the electrolyzer, which converts hydrogen and oxygen to produce energy and water.

This paper presents an economic analysis of a small-scale SAPV system with HSS for a predefined residential load demand. A case study was conducted using Kuala Lumpur's meteorological data and typical rural area daily load profile of 2.215 kWh. Detail configuration, system sizing, and economic analysis were performed and also discussed. Finally, the levelized cost of energy (LCOE) of the proposed system was determined. The new concept in this contribution introduces the integration of PV with HSS, with prior information, assessment, and extensive sizing steps on each component with respect to the site's local environment (or climate condition). It is important so that it meets the design requirement of the plant installation (load demand). An economic analysis was carried to determine the system feasibility and economically utilize the PV and HSS system [7, 8].

## 2.0 SYSTEM CONFIGURATION

The proposed configuration for an SAPV system with HSS in Malaysia is shown in Fig. 1. During daytime, the PV system generates DC power. If a PV array produces higher power than load demand, the surplus power goes to an electrolyzer. The electrolyzer uses the excess power to convert water into hydrogen and oxygen. The hydrogen is stored in a hydrogen tank and oxygen is released into the air. However, during insufficient PV power, FC draws hydrogen from the storage tank and oxygen from the air, and converts both gases into water again to produce more power to serve load demand. Meanwhile, an inverter is used to convert DC power into AC power [9, 10].

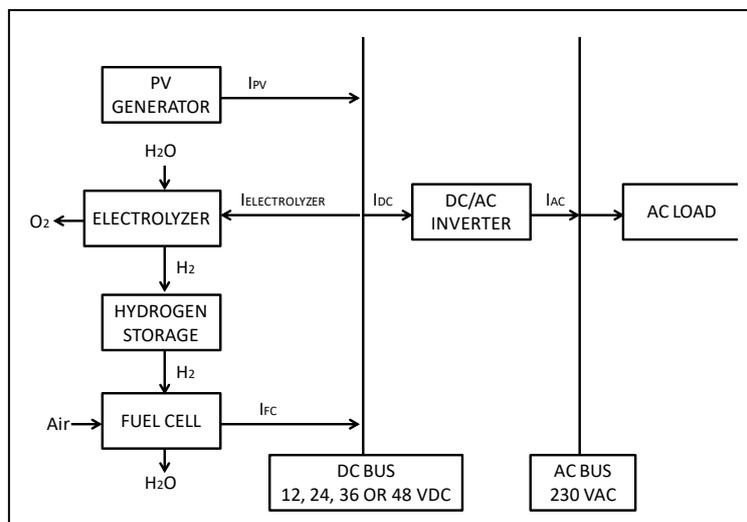


Figure 1. System configuration for an SAPV system with HSS [9, 10]

## 2.1 Solar Energy Resources

Predicting PV accuracy has a great importance in sizing process. This is because the energy generated by a PV system is forecasted from the site's weather data [11]. The average monthly annual irradiation and PSH data for Kuala Lumpur were generated by Meteonorm 6.1 as shown in Table 1 [12]. It was observed that the annual global irradiation for Kuala Lumpur was 1,655.59 kWh/m<sup>2</sup>, the maximum average annual irradiance over a year,  $H_{Smax}$  was 205.511 W/m<sup>2</sup> (March), and the lowest monthly daily's peak sun hour,  $PSH_{lowest}$  was 4.081 hr/day (December).

**Table 1.** Monthly average annual irradiation and daily's peak sun hour in Kuala Lumpur [12]

Month	Average Annual Irradiance (W/m <sup>2</sup> )	PSH (hr)	Month	Average Annual Irradiance (W/m <sup>2</sup> )	PSH (hr)
January	179.839	4.319	July	188.978	4.535
February	202.976	4.871	August	186.962	4.487
March	205.511	4.945	September	187.778	4.513
April	199.861	4.800	October	190.860	4.584
May	194.892	4.681	November	171.944	4.127
June	187.639	4.513	December	170.027	4.081

## 2.2 Load Demand

Table 2 presents the residential load demand in Malaysia's rural area. It is assumed that the daily load remains the same throughout the year [13]. The AC load profile of 2.215 kWh consists of different types of home appliances.

**Table 2.** Common daily load profile for a house in a rural area

Appliance	Voltage (V)	Power (W)	Daily Usage (hr)	Energy (Wh)
Lamp 1	230	20	10	200
Lamp 2	230	40	4	160
Television	230	60	5	300
Refrigerator	230	50	24	1200
Radio	230	10	11	110
Ceiling Fan	230	60	2	120
Desk Fan	230	25	5	125
Total		265		2,215

## 3.0 SYSTEM DESIGN

This section explains the design steps and the calculation needed to determine the required capacity for SAPV components by using amp-hour analysis. The advantage of amp-hour analysis is it considers the actual components' behavior [14].

### 3.1 Estimation of Load Profile

First, the total daily energy requirement was estimated. All AC equipment including their rated power and the total usage in hours per day was listed. After that, the daily AC load demand,  $E_{AC}$  was determined. Additional energy was also considered to cover losses by components' inefficiencies. The estimation of energy losses and total daily energy requirement was calculated by using Equation 1 and 2 ( $\eta_{AClosses} = 0.35$ ) [14]. The daily system charge requirement,  $Q_{req}$  (Ah) was calculated using Equation 3, where  $V_{DCbus}$  is the DC bus voltage.

$$AC_{losses} = E_{AC} * \eta_{AClosses} \tag{1}$$

$$E_{req} = E_{AC} + AC_{losses} \tag{2}$$

$$Q_{req} = \frac{E_{req}}{V_{DCbus}} \tag{3}$$

### 3.2 Sizing of PV Array

In sizing of PV arrays, designers have to estimate site’s meteorological data. Sizing calculation by using the lowest monthly PSH (hr),  $PSH_{lowest}$ , actually prevents the system to be undersized. The array sizing needs to be aligned with the load demand. Hence, from the value obtained from Equation 3,  $Q_{req}$  (Ah), the system charging current by PV array,  $I_{charge}$  (A) was determined by Equation 4 [14].

$$I_{charge} = \frac{Q_{req}}{PSH_{lowest}} \quad (4)$$

The modules connection was arranged based on the preselect PV model’s technical data [15]. Equation 5 was used to determine the number of parallel string,  $N_p$ , where  $I_{mp}$  is the PV current maximum power. Next, series-connected panels in each parallel string,  $N_{mod/strg}$ , were calculated by Equation 6, where  $V_{mod\_rated}$  is the PV rated voltage. Lastly, the total PV modules,  $N_{pv}$ , were determined by Equation 7 [14]:

$$N_p = roundup \left( \frac{I_{charge}}{I_{mp}} \right) \quad (5)$$

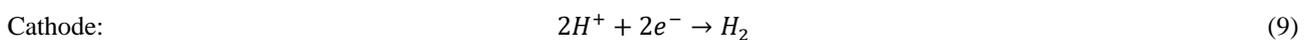
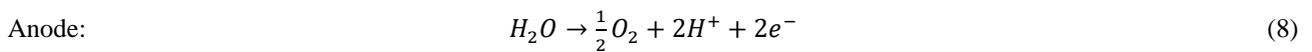
$$N_{mod/strg} = \frac{V_{od\_rated}}{V_{DCbus}} \quad (6)$$

$$N_{pv} = N_p * N_{mod/strg} \quad (7)$$

### 3.3 Sizing of Proton Exchange Membrane Electrolyzer

The preferable and most common technologies used in water electrolyzers are alkaline and PEME. Commercially available PEME can produce from 400–7,900 kg of hydrogen each year with pressure generation up to 13.8 bar. Meanwhile, an alkaline electrolyzer produces 2400–71,000 kg of hydrogen over a year. The advantage of PEME technology is it has high energy efficiency for each stack (75–88%) with 5% as the minimum required output flow for a safe operation [4].

An electrolyzer decomposes water into hydrogen and oxygen by passing electrical current (i.e. DC) between two electrodes separated by an aqueous electrolyte with good ionic conductivity. The reactions take place at the anode and the cathode of an electrolyzer are as follows [16]:



The storage charge capacity required,  $Q_{stored}$  was determined by Equation 10 [14, 17], where  $N_c$  is the number of reserved days and  $DOD$  is the depth of discharge.  $N_c$  was set between 1 and 4 days, and it is recommended that  $DOD$  should not be more than 60%. Energy storage consumption,  $E_{storeq}$  is the amount of energy consumed to produce stored hydrogen and was calculated using Equation 11, where  $\eta_{Elz}$  is the electrolyzer efficiency and  $\eta_{FC}$  is the FC efficiency ( $\eta_{Elz} = 0.88$  and  $\eta_{FC} = 0.6$ ).

$$Q_{stored} = \frac{Q_{req} * N_c}{DOD} \quad (10)$$

$$E_{stored} = \frac{Q_{stored} * V_{DCbus}}{\eta_{Elz} * \eta_{FC}} \quad (11)$$

Meanwhile, the electrolyzer rated power,  $P_{Elz}$  is equal to the maximum excess in the PV generation power over the minimum load power, where  $A_{PV}$  is the PV panel area and  $\eta_{PV}$  is the PV panel efficiency [4, 18].

$$P_{Elz} = H_{Smax} * A_{PV} * \eta_{PV} \quad (12)$$

### 3.4 Sizing of H<sub>2</sub> Storage Tank

Hydrogen can be stored in liquid or gas condition. Liquid hydrogen is stored in cryogenic tanks and gaseous hydrogen is stored in either medium or high-pressure cylinders or near atmospheric pressure in metal hydrides. The hydrogen formed by the electrolyzer during each month is calculated by assuming the produced hydrogen is stored completely before it supplies power to the residential load. The amount of hydrogen produced annually is the total excess of PV power transformed into volume, which is expressed in m<sup>3</sup> [18].

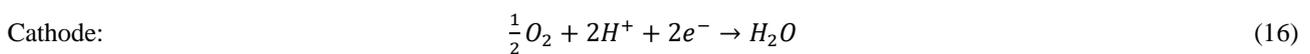
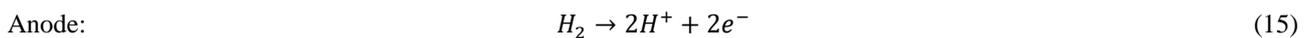
Equation 13 represents the hydrogen mass required to produce the specific electrical energy,  $m_{h_2}$  where  $HHV$  is the higher heating value of hydrogen (39.44 kWh/kg). The hydrogen's required volume capacity,  $V_{h_2}$  was calculated in the next equation, where  $M_c$  is the margin coefficient for a compressor and storage hydrogen leakage compensation, and  $\rho_{h_2}$  is the hydrogen density. The value of  $M_c$  is greater than 1.1 and  $\rho_{h_2}$  is 0.089 kg/m<sup>3</sup> [4].

$$m_{h_2} = \frac{E_{stored}}{HHV} \quad (13)$$

$$V_{h_2} = \frac{m_{h_2}}{M_c * \rho_{h_2}} \quad (14)$$

### 3.5 Sizing of Proton Exchange Membrane Fuel Cell

The reverse reaction occurs in an electrolyzer takes place in FC. Hydrogen in the anode is ionized, releasing electrons and protons. Electrons flow to the cathode through a circuit, producing electric current. Protons diffuse through a polymer electrolyte membrane and react at the cathode with oxygen and electrons to form water. The chemical reactions happened in a proton exchange membrane fuel cell (PEMFC) as below [16]:



The following equation is for FC sizing by considering the maximum AC load power in the household, where  $M_{FC}$  is the margin coefficient of FC,  $P_{ACload}$  is the total AC load power, and  $\eta_{inv}$  is the inverter efficiency [18].

$$P_{FC} = M_{FC} * \frac{P_{ACload}}{\eta_{inv}} \quad (17)$$

### 3.6 Sizing of Inverter

An inverter is supposed to convert DC supply and fulfill the maximum AC load in a household. Hence, inverter power rating,  $P_{inv}$  was determined using Equation 18, where 1.25 is an oversized factor [19].

$$P_{inv} = P_{ACload} * 1.25 \quad (18)$$

#### 4.0 ECONOMIC ANALYSIS

Economic analysis determines the viability of the proposed system. In this paper, life-cycle cost (LCC) and LCOE were used to analyze the feasibility of the system. LCC is the present value of installation cost, operating and maintenance cost, and replacement cost [20]. Equation 19 presents LCC equation, where  $C_{pv}$  is the solar array cost,  $C_{storage}$  is the HSS cost,  $C_{inv}$  is the inverter cost,  $C_{install}$  is the installation cost,  $C_{invrep}$  is the present value of inverter replacement,  $C_{O\&M\_20years}$  is the present value of operation and maintenance cost (1% from the initial cost), and  $C_{salvage}$  is the salvage value (20% from the initial cost). All components have 20 years of lifetime, besides the inverter (inverter lifetime = 10 years) [21, 22].  $N$  is the project's period and  $i$  is the market rate.

$$LCC = C_{pv} + C_{inv} + C_{controller} + C_{install} + C_{invrep} + C_{O\&M\_20years} + C_{salvage} \quad (19)$$

$$C_{invrep} = C_{inv} \left( \frac{i}{1+i} \right)^N \quad (20)$$

$$C_{O\&M\_20years} = C_{O\&M} * \left[ \frac{\left( \frac{i}{1+i} \right)^N - 1}{i * \left( \frac{i}{1+i} \right)^N} \right] \quad (21)$$

Market interest rate,  $i$  was determined using Equation 22, where  $i'$  is the real interest rates.  $i'$  was calculated using Equation 23 [23], where  $BLB$  is the base lending rates, and  $\bar{f}$  is the inflation rate [24, 25].

$$i = i' + \bar{f} - i' * \bar{f} \quad (22)$$

$$i' = BLB - 2\% \quad (23)$$

LCOE (RM/kWh) is the average cost per kWh of electrical energy produced by a PV array [26]. It was calculated by dividing annualized life-cycle cost,  $LCC_{1year}$  with the total useful electrical energy generated,  $E_{pv}$ , as calculated by the following equations [27]. Table 3 summarizes the market prices for the system components [4, 8,22, 28-31].

$$LCC_{1year} = \frac{LCC}{\left[ \frac{\left( \frac{i}{1+i} \right)^N - 1}{i * \left( \frac{i}{1+i} \right)^N} \right]} \quad (24)$$

$$LCOE = \frac{LCC_{1year}}{E_{pv}} \quad (25)$$

$$E_{pv} = N_{pv} * P_{mp\_STC} * PSH_{year} * \eta_{losses} \quad (26)$$

**Table 3.** Pricing of components [4, 8, 22, 28-31]

Components	Unit	RM
Solar Panel, 140 W	1	886.17
Inverter, 340 W	1	560.71
PEME	RM/W	4.44
H <sub>2</sub> Storage Tank	RM/Nm <sup>3</sup>	77.88
PEMFC	RM/W	1.02
Support Structure & Installation Cost	RM/Wp	4.00

## 5.0 RESULTS AND DISCUSSION

This section presents the system sizing results, economic analysis for 20 years period, feasibility comparison between SAPV with HSS and SAPV with absorbent glass mat (AGM) battery, and sensitivity analysis of LCOE value for SAPV with HSS towards  $\eta_{elz}$  and  $\eta_{fc}$  values.

### 5.1 Sizing Results

Table 4 below shows the results of system sizing and each component’s technical data. A combination of 1.12 kWh PV modules, 335.4 W PEME, 324.3 Nm<sup>3</sup> H<sub>2</sub> tank, 285.0 W PEMFC, and 340 W inverter were chosen as the proposed system.

**Table 4.** Proposed system sizing

Daily Energy Requirement		
Total Daily AC Energy Demand	2,215.00	Wh
AC Losses	775.25	Wh
Total Daily Energy Required	2,990.25	Wh
System Voltage	24.00	VDC
Daily Charge Required	124.59	Ah
Sizing of PV Modules		
Lowest Daily's Peak Sun Hour	4.08	hr
System Design Charging Current	30.53	Amp
Model	Kyocera KD140	
Peak Watts	140.00	Wp
Rated Voltage	12.00	VDC
Maximum Power Rated Current	7.91	Amp
Short Circuit Current	8.68	Amp
PV Efficiency	20.40	%
Number of Parallel String	4	
Number of Modules/String	2	
Number of Modules	8	
PV Array Area	8.016	m <sup>2</sup>
Sizing of Hydrogen Storage System		
Daily System Charge Requirement	124.59	Ah
Reserve Days	2	day
Maximum DOD	50	%
Required System Storage Capacity	498.38	Ah
Energy Storage of Electrolyzer	22,653.4	Wh
Rated Power of Electrolyzer	335.409	W
Mass of Hydrogen Stored	5.63463	N
Volume of Hydrogen Stored	57.555	m <sup>3</sup>
Hydrogen Tank Capacity	324.301	Nm <sup>3</sup>
Rated Power of Fuel Cell	284.946	W
Sizing of Inverter		
Maximum Power AC Load	265	W
Inverter Rating	340	W
Model	Cotek SK350-224	
Rated Voltage	24/230	VDC/VAC
Rated Power	350	W
Inverter Efficiency	93	%

## 5.2 Economic Analysis

Table 5 below presents the economic analysis for the proposed configuration. From the analysis, the total initial cost for equipment, installation, and structure was RM39,559.79. The present values of operation & maintenance and replacement cost were RM3,884.06 and RM259.72, respectively. The approximated salvage value was RM7,911.96. Hence, LCC for 20 years was RM35,791.61, and  $LCC_{1year}$  was RM3,645.46.  $E_{PV}$  for the proposed system was 1,828.305 kWh. Consequently, LCOE calculated was RM1.98/kWh.

**Table 5.** Economic analysis

Discount/Interest Rates	4.60%
Inflation Rates	3.40%
Net Discount Rates, $i$	8.00%
<b>Components</b>	<b>RM</b>
<b>Initial Cost</b>	
PV Module(s)	7,089.36
Electrolyzer	1,489.40
H <sub>2</sub> Storage Tank	11,225.17
PEMF	292.00
Inverter	560.71
Module Support Structure & System Installation	4,480.00
Contingencies	391.69
Total Initial Cost	39,559.79
<b>O&amp;M Cost</b>	
LCC O&M <sub>m</sub>	395.60
Total Operation & Maintenance	3,884.06
<b>Replacement Cost</b>	
LCC Inverter <sub>n1</sub> (Replacement after 10 years)	259.72
Total Replacement Cost	259.72
<b>Salvage</b>	
Total Salvage Value	7,911.96
<b>Result</b>	
LCC Cost for 20 Years	35,791.61
LCC Cost/Year	3,645.46
Cost of Energy (RM/kWh)	1.98

## 5.3 Comparison with Standalone Photovoltaic/Absorbent Glass Mat Battery System Sizing

The current results were compared with the findings from an SAPV system with AGM battery, which was published in 2014 [28]. Table 6 shows the comparison of the current findings with the published results. From the published literature, the initial cost for the SAPV system with AGM battery was RM39,559.79, the LCC value was RM34,232, the  $LCC_{1year}$  was RM3,206.82, and the system's LCOE was RM1.76/kWh.

From the comparison, it can be seen that the initial cost, the LCC, the annual LCC, and the LCOE for SAPV with HSS have higher expenditure compared to the published findings [28]. The LCOE for SAPV with HSS was higher by 12.5%. This is because the initial cost needed for HSS is very high as FC efficiency is quite low (60%). Consequently, bigger HSS capacity is needed to have backup energy similar with an AGM battery during insufficient PV generation.

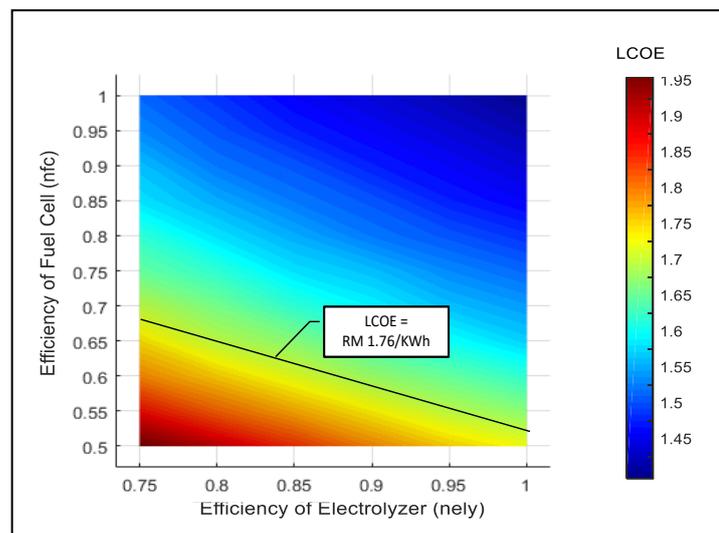
However, SAPV with AGM battery has a flaw. The AGM battery needs to be replaced every 5 years. Meanwhile, PEME, H<sub>2</sub> tank, and PEMFC do not have to be replaced because the lifetime is longer, which is 20 years [18]. Hence, SAPV with HSS could be compatible with SAPV with AGM battery if  $\eta_{elz}$  and  $\eta_{fc}$  values increase in the future.

**Table 6.** Comparison of SAPV with HSS and SAPV with AGM battery

Economic Analysis Results	SAPV with Hydrogen Storage	SAPV with AGM Battery [9]
Initial Cost (RM)	39,559.79	21,393.75
LCC Cost for 25 Years (RM)	35,791.61	34,231.98
LCC Cost/Year (RM/year)	3,645.46	3,206.81
LCOE (RM/kWh)	1.98	1.76
LCOE Percentage Difference	Increased by 12.5%	

#### 5.4 Sensitivity Analysis

The sensitivity of LCOE value for SAPV with HSS depends on  $\eta_{elz}$  and  $\eta_{fc}$ . The effect of  $\eta_{elz}$  and  $\eta_{fc}$  values for a range between 0.75 and 1.00, and 0.50 and 1.00 towards system’s LCOE was analyzed. The sensitivity analysis is portrayed in Fig. 2 below.



**Figure 2.** Effect of  $\eta_{elz}$  and  $\eta_{fc}$  on LCOE value for SAPV with HSS

The figure above presents a curve of  $\eta_{elz}$  and  $\eta_{fc}$  combination and its effect on LCOE value for SAPV with HSS. Based on the figure, for a specific LCOE value (e.g. RM1.76/kWh), the relation between  $\eta_{elz}$  and  $\eta_{fc}$  is approximately linear and can be presented by Equation 27 below:

$$\eta_{fc} = (-0.627) * \eta_{elz} + 1.149 \tag{27}$$

The graph curve and the equation above can be used as references or benchmarks to find the combination of  $\eta_{elz}$  and  $\eta_{fc}$  with LCOE value lower than SAPV with AGM battery. The mitigation of  $\eta_{elz}$  and  $\eta_{fc}$  value is important, so that an SAPV system with HSS can compete with the conventional SAPV system with AGM in the future.

#### 6.0 CONCLUSION

A sizing and economic analysis of a small-scale SAPV with HSS was carried out. Based on the economic assessment, it was found that the LCC for the proposed system, the annual LCC, and the LCOE value obtained were RM35,791.61, RM3,645.46, and RM1.98/kWh, respectively.

However, compared to the economic analysis of SAPV with AGM battery from a published literature [28], the expenditure for the system was lower, where the LCC for the system was RM34,232 and the annual LCC was RM3,206.82. The LCOE value for the SAPV system with AGM battery was lower than the proposed system by 12.5%, which was RM1.76/kWh. It can be seen that even though hydrogen has high energy density per mass, it has low efficiency

as a storage system and expensive. Due to the low efficiency storage, designers need to store hydrogen storage's energy capacity higher than the AGM battery. However, as an emerging commercialize product, the manufacturers and researchers can focus on how to increase storage system efficiency for future usage. The HSS round-up trip efficiency must improve dramatically before they can offer the same overall energy efficiency as batteries.

Therefore, a sensitivity analysis was performed to find a reference or benchmark value of an electrolyzer and FC efficiencies with the LCOE value lower than SAPV with AGM battery. In order to obtain the LCOE lower than SAPV with AGM battery, a curve and an equation were developed to present the relation between  $\eta_{elc}$  and  $\eta_{fc}$  for a predefined LCOE value (RM1.76/kWh). This finding is crucial to envisage the applicability of SAPV with HSS for future power generation in Malaysia.

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